

Math 521 Lecture #9  
§1.3.2: Stability and Bifurcation, Part II

**Example 1.25.** We model a plant-herbivore system and determine its bifurcation diagram.

We assume that the plant biomass  $P(t)$  grows logistically with growth rate  $r$  and carrying capacity  $K$ .

We assume there are a fixed number  $H$  of herbivores who consume plant biomass at the rate of

$$\frac{aP}{1 + bP}$$

per herbivore, where  $a$  has dimensions of per time per herbivore and  $b$  has dimensions of per plant biomass.

The consumption rate of the herbivores limits to  $a/b$  as  $P \rightarrow \infty$ .

Under the assumptions, a model for the plant-herbivore system is

$$\frac{dP}{dt} = rP \left(1 - \frac{P}{K}\right) - \frac{aP}{1 + bP}H.$$

There are five parameters in this model, namely  $r$ ,  $K$ ,  $a$ ,  $b$ , and  $H$ .

We non-dimensionalize the model through the dimensionless quantities

$$\tau = rt, \quad N = \frac{P}{K}.$$

The model then becomes

$$\frac{dN}{d\tau} = N(1 - N) - \frac{hN}{1 + cN}$$

for the two dimensionless parameters

$$h = \frac{aH}{r}, \quad c = Kb.$$

It is reasonable to assume that the plant biomass has a large carrying capacity, so that we can safely assume  $c > 1$  and fixed.

Our interest is in what happens as the number of herbivores varies, so  $h$  is the bifurcation parameter.

An equilibrium  $N^*$  of the model is a solution of

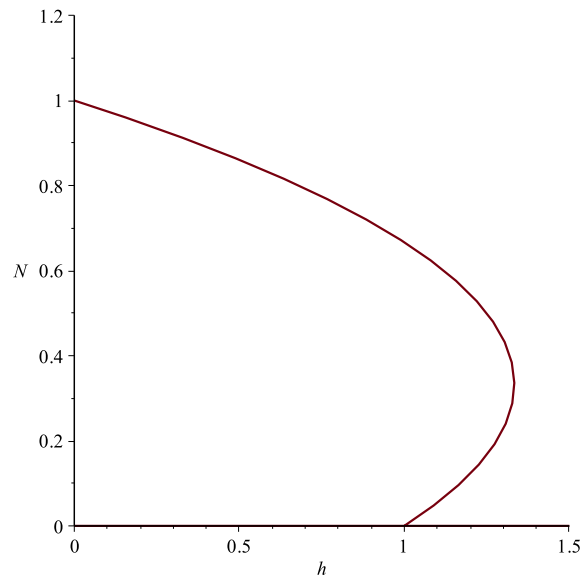
$$N^* \left[ (1 - N^*) - \frac{h}{1 + cN^*} \right] = 0.$$

This gives  $N^* = 0$  (for all values of  $h$ ) and the solutions (if any) of

$$(1 - N^*)(1 + cN^*) - h = 0.$$

We could solve this for  $N^*$  explicitly (via the quadratic formula) as functions of  $h$  and plot these curves.

Instead we plot the curve  $h = (1 - N^*)(1 + cN^*)$ , which gives the same thing, along with  $N^* = 0$ . [The nontrivial curve is for  $c = 3$ .]



Notice that  $h = 0$  when  $N^* = 1$  and  $h = 1$  when  $N^* = 0$  (regardless of the value of  $c$ ).

The largest value of  $h$  for which there is an equilibrium can be found by setting the derivative of  $h = (1 - N^*)(1 + cN^*)$  (with respect to  $N^*$ ) to zero:

$$h = \frac{(c + 1)^2}{4c} \text{ at } N^* = \frac{c - 1}{2c}.$$

Through geometric analysis, we learn that each equilibrium on the 0 branch on the bifurcation diagram is unstable for  $0 < h < 1$  and locally asymptotically stable for  $h > 1$ .

Each equilibrium on the upper branch (starting at  $(0, 1)$  and down to the “top” of the parabola) is locally asymptotically stable, while on the lower branch (from the “top” of the parabola down to the point  $(1, 0)$ ) is unstable.

The bifurcation diagram includes the words “stable” on the locally asymptotically stable branches, and “unstable” on the unstable branches.

For  $h > (c + 1)^2/4c$ , the locally asymptotically stable equilibrium at  $N^* = 0$  is globally asymptotically stable, i.e., every solution has the property that  $N \rightarrow 0$  as  $t \rightarrow \infty$ .

**Example 1.27.** We model a non-isothermal tank reactor for determining the temperature  $\bar{\theta}$  and the concentration  $\bar{c}$  of a heat-releasing, chemically reacting substance.

We assume that the tank is continuously stirred to maintain a uniform temperature and uniform chemical concentration.

The tank, of fixed volume  $V$ , is continuously fed a chemical reactant at concentration  $c_i$  and temperature  $\theta_i$  in a stream with constant flow rate  $q$ .

After mixing and reacting, the products are removed at the same flow rate  $q$ .

We assume the exothermal reaction is first-order and irreversible, and that the reactant disappears at the rate of

$$-k\bar{c}e^{-A/\bar{\theta}}$$

for constants  $A$  (with dimension temperature) and  $k$  (with dimension per time).

We assume the amount of heat released is given by

$$hk\bar{c}e^{-A/\bar{\theta}}$$

where  $h$  is a positive constant (the specific heat of reaction) measured in energy per mass.

We have two quantities to model, the concentration  $\bar{c}(\bar{t})$  and the temperature  $\bar{\theta}(\bar{t})$ .

For the concentration, we use mass balance to obtain

$$V\frac{d\bar{c}}{d\bar{t}} = qc_i - q\bar{c} - Vk\bar{c}e^{-A/\bar{\theta}}.$$

For the temperature, we use heat balance to obtain

$$VC\frac{d\bar{\theta}}{d\bar{t}} = qC\theta_i - qC\bar{\theta} + hVk\bar{c}e^{-A/\bar{\theta}}$$

where  $C$  is the heat capacity of the mixture, measured in energy per volume per temperature.

To non-dimensionalize these equations, we introduce the dimensionless variables

$$t = \frac{\bar{t}}{V/q}, \quad \theta = \frac{\bar{\theta}}{\theta_i}, \quad c = \frac{\bar{c}}{c_i},$$

and the dimensionless parameters

$$\mu = \frac{q}{kV}, \quad b = \frac{hc_i}{C\theta_i}, \quad \gamma = \frac{A}{\theta_i}.$$

The system of two first-order equations becomes

$$\begin{aligned} \frac{dc}{dt} &= 1 - c - \frac{ce^{-\gamma/\theta}}{\mu}, \\ \frac{d\theta}{dt} &= 1 - \theta + \frac{bce^{-\gamma/\theta}}{\mu}. \end{aligned}$$

At first glance, it looks impossible to solve this nonlinear systems of ODEs.

But if we multiply the first one through by the constant  $b$ , and add this to the second equation we get

$$\frac{d(\theta + bc)}{dt} = 1 + b + (\theta + bc).$$

This integrates to

$$\theta + bc = 1 + b + De^{-t}$$

for a constant  $D$ .

Assuming that  $\theta + bc$  at  $t = 0$  is  $1 + b$ , the constant  $D$  takes the value 0, so that  $\theta + bc = 1 + b$ . [This choice of initial condition is to insure the resulting equation is autonomous.]

Thus  $bc = 1 + b - \theta$ , so the the heat balance equation becomes

$$\frac{d\theta}{dt} = 1 - \theta - \frac{(1 + b - \theta)e^{-\gamma/\theta}}{\mu}.$$

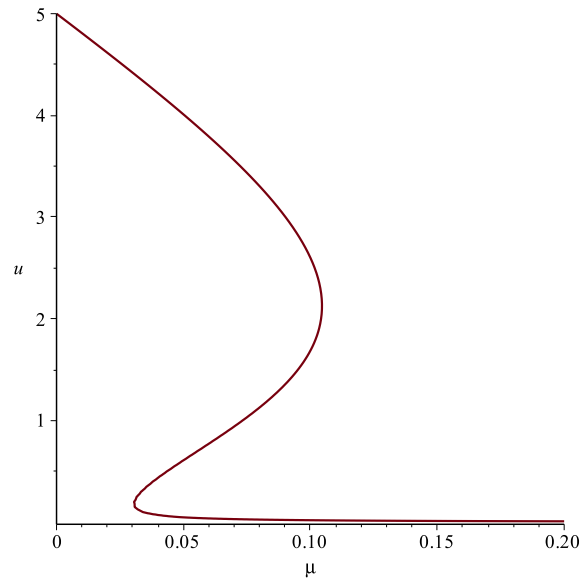
Changing the dependent variable by  $u = \theta - 1$  gives

$$\frac{du}{dt} = -u + \frac{(b - u)e^{-\gamma/(u+1)}}{\mu} = \frac{-\mu u + (b - u)e^{\gamma/(u+1)}}{\mu}.$$

The parameter  $\mu$  is the ratio of the flow rate  $q$  and the reaction rate  $kV$ .

Fixing the parameters  $b$  and  $\gamma$ , we use  $\mu$  as a bifurcation parameter.

Solving the equation for its equilibrium solutions is not possible in an analytic manner, so instead we use numerical methods to plot the curve in the bifurcation diagram. [The curve is for  $b = 5$  and  $\gamma = 8$ .]



A geometric analysis reveals that the equilibrium is locally (globally if  $\mu$  small enough) asymptotically stable on the branch connecting  $(0, 5)$  to the first vertical tangent, unstable from the first vertical tangent to the second vertical tangent, and locally (globally if  $\mu$  large enough) asymptotically stable on the remainder part of the curve.